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(54) DISTILLATION EQUIPMENT FOR PRODUCING SPONGE TITANIUM

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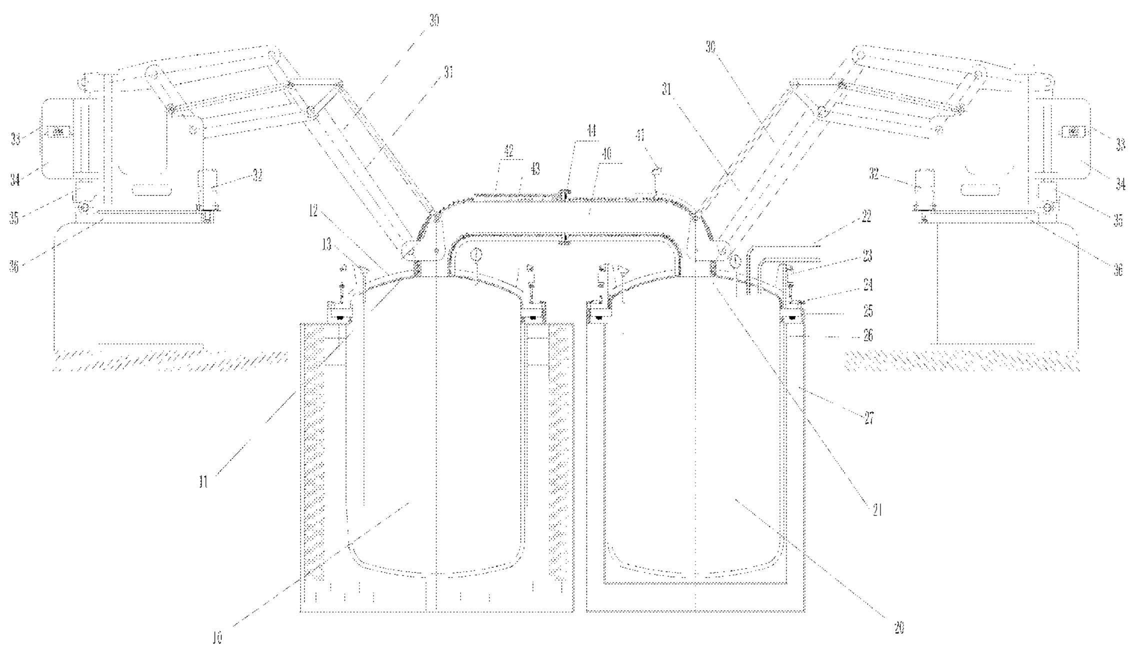
(57) **ABSTRACT**

The present invention provides a piece of distillation equipment for producing sponge titanium, which includes a heating furnace and a reactor for containing a condensate, wherein a heating furnace cover is arranged above the heating furnace, a reactor cover is arranged above the reactor, the heating furnace cover is connected with the reactor cover by a pipe, a resistance wire is arranged on the pipe, each lifting device is arranged above the heating furnace cover and the reactor cover, a vacuum-pumping pipe is arranged above a heater cover, and a first metal sealing ring is arranged between the reactor cover and the reactor. The present invention has the beneficial effects that the distillation equipment can ensure normal production, and effectively ensure the quality of sponge titanium product. The problem of distillation tube blockage is solved by adopting a metal gasket.



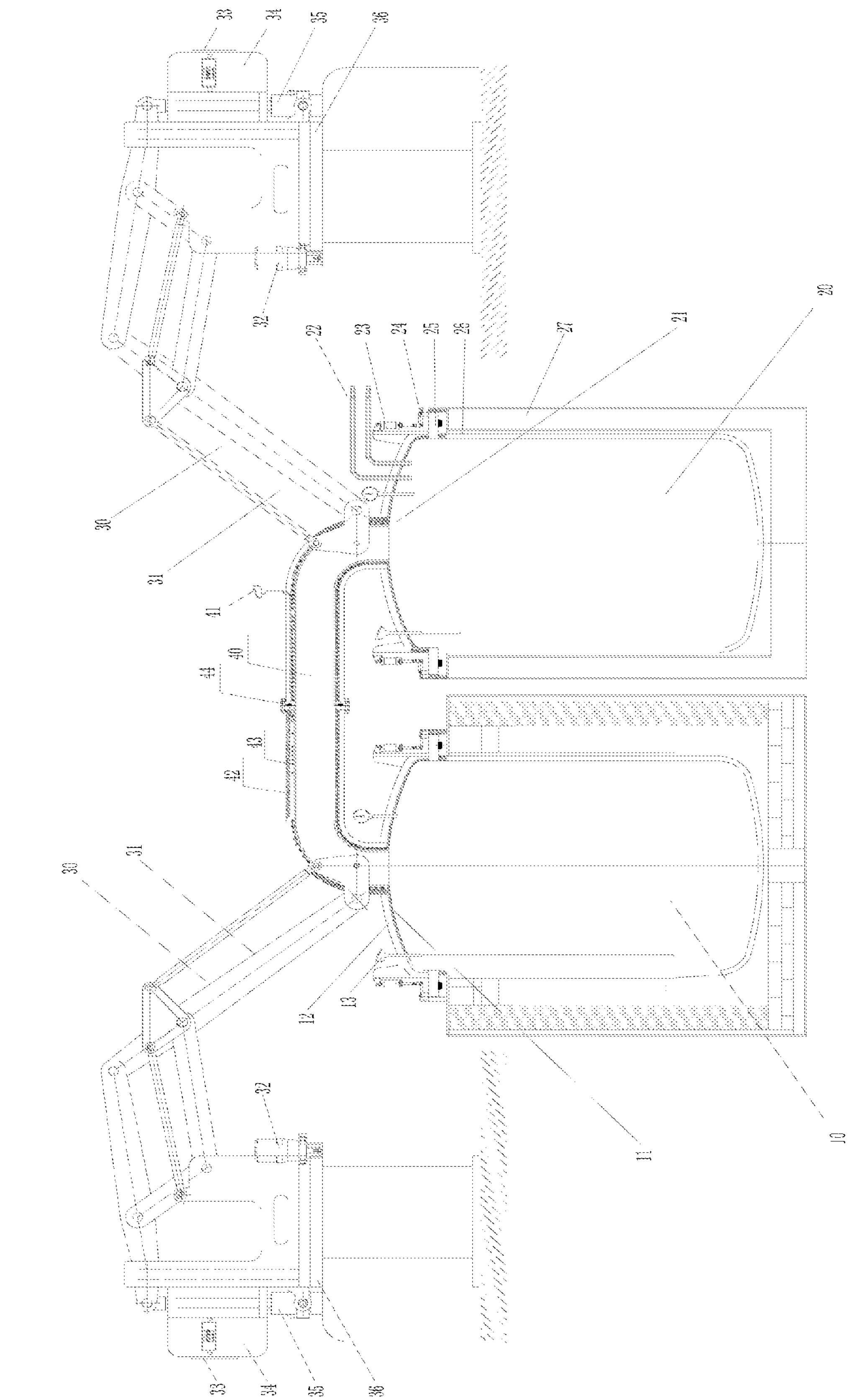


FIG. 1

DISTILLATION EQUIPMENT FOR PRODUCING SPONGE TITANIUM

TECHNICAL FIELD OF THE INVENTION

[0001] The present invention relates to a piece of distillation equipment for producing sponge titanium, and in particular to a piece of distillation equipment for producing sponge titanium, which is easy to operate and energy-saving.

BACKGROUND OF THE INVENTION

[0002] The main technical routes for producing high quality sponge titanium include: 1. studying a process and equipment for preparing high-purity magnesium to enable fine magnesium to reach the requirements for the production of high quality sponge titanium; 2. studying a process and equipment for preparing deeply purified fine titanium tetrachloride to enable the fine titanium tetrachloride to reach the requirements for the production of high quality sponge titanium; 3. studying a process for improving the vacuum degree of vacuum system and the tightness of reduction distillation equipment; 4. studying a process and equipment for reduction distillation and finished product breaking to produce a satisfactory high quality sponge titanium.

[0003] At present, the production process of sponge titanium at home and abroad mainly adopts metallothermic reduction process, and in particular refers to preparing metal M from metal reducing agent (R) and metal oxide or chloride (MX). Titanium metallurgy method in which industrial production has been achieved is magnesiothermic reduction process (Kroll process) and sodiothermic reduction process (Hunter process). Since the Hunter process leads to higher production cost than the Kroll process does, the Kroll process is widely used in industry currently. The main processes of the Kroll process are that magnesium ingot is placed into a reactor, heated and molten after being subjected to oxide films and impurities removal, then titanium tetrachloride ($TiCl_4$) is introduced into the reactor, titanium particles generated by the reaction are deposited, and generated liquid magnesium chloride is discharged promptly through a slag hole. The reaction temperature is usually kept at 800° C. to 900° C., the reaction time is between several hours and several days. Residual metallic magnesium and magnesium chloride in end product can be removed by washing with hydrochloric acid, can also be removed by vacuum distillation at 900° C., and keep the purity of titanium high. The Kroll process has the disadvantages of high cost, long production cycle, and polluted environment, limiting further application and popularization. At present, the process has not changed fundamentally, and still belongs to intermittent production, which fails to realize continuous production, and there is no corresponding improved equipment developed, which is not conducive to further development of sponge titanium manufacturing technology.

SUMMARY OF THE INVENTION

[0004] In order to solve the shortcomings of high cost, severe pollution and long production cycle in prior art, the present invention provides a method for producing sponge titanium technically:

[0005] Scheme 1: a method for preparing titanium from potassium fluotitanate with aluminothermic reduction process:

[0006] Equation involved: $3K_2TiF_6+4Al=3Ti+6KF+4AlF_3$

[0007] Scheme 2: a method for preparing sponge titanium from potassium fluotitanate with magnesiothermic reduction process:

[0008] Equation involved: $K_2TiF_6+2Mg=Ti+2MgF_2+2KF$

[0009] Scheme 3: a method for preparing sponge titanium from potassium fluotitanate with aluminum magnesium thermal reduction process:

[0010] Equations involved:

[0011] $3K_2TiF_6+4Al=3Ti+6KF+4AlF_3$

[0012] $K_2TiF_6+2Mg=Ti+2MgF_2+2KF$

[0013] Since the potassium fluotitanate, aluminum and magnesium are solids in the raw material, which are different from the traditional production process, the present invention provides a piece of distillation equipment for producing sponge titanium, which includes: a heating furnace and a reactor for containing a condensate, wherein a heating furnace cover is arranged above the heating furnace, a reactor cover is arranged above the reactor, the heating furnace cover is connected with the reactor cover by a pipe, a resistance wire is arranged on the pipe, each lifting device is arranged above the heating furnace cover and the reactor cover, a vacuum-pumping pipe is arranged above a heater cover, and a first metal gasket and a second metal gasket are respectively arranged between two ends of the pipe and the heating furnace cover and the reactor cover.

[0014] The present invention, by adopting the above technical schemes, is advantaged in that the pipe is densely provided with resistance wires, particularly the resistance wires are arranged at the corner of the pipe, so that during distillation, distilled products do not coagulate in the pipe to avoid blockage, the distillation efficiency is improved, the equipment avoids the cooling of vacuum distillation in traditional method, saves time and electricity, in addition, each lifting device is arranged above the reactor and the heating furnace, which makes the operation easy and greatly saves labor. Moreover, the product does not come into contact with air, avoiding the possibility that the sponge titanium comes into contact with oxygen and improving the quality of product.

[0015] Preferably, the first metal gasket has a softening point of 900° C. and a melting point of 1000° C., and the second metal gasket has a softening point of 1100° C. and a melting point of 1200° C.

[0016] The present invention, by further adopting the above technical characteristics, is advantaged in that, in the distillation equipment of the present invention, the temperature in the heating furnace is usually 850° C. to 950° C., the temperature in the reactor is usually 1000° C., the above metal gasket can be used for further ensuring the tightness during distillation and improving the distillation speed.

[0017] Preferably, the inner wall of the reactor is provided with a metal crucible and a water-cooling jacket for cooling.

[0018] Preferably, the reactor cover is also provided with a locking mechanism fixedly connected with the reactor and a locking cylinder for providing power for the locking mechanism.

[0019] The present invention, by further adopting the above technical characteristics, is advantaged in that the reactor is kept under a condition of totally sealing to further improve the distillation efficiency.

[0020] Preferably, the lifting device includes a vertical lifting structure connected with the reactor cover, a lifting hydraulic cylinder for providing power and a hydraulic steering motor for adjusting the lifting hydraulic cylinder are arranged below the vertical lifting structure.

[0021] Preferably, a first thermocouple and an insulation material are arranged on the heating furnace cover.

[0022] Preferably, the upper and lower ends of the pipe are provided with metal sealing rings.

[0023] Preferably, a touch screen and an electric cabinet for controlling the movement of the lifting device are arranged above the lifting hydraulic cylinder.

[0024] Preferably, a pivoting support is arranged below the electric cabinet.

[0025] Preferably, the pipe is provided with a second thermocouple, an insulation layer and a heating wire orderly.

[0026] The present invention has the beneficial effects that, by adopting the above technical schemes, the production equipment can ensure normal production, and effectively ensure the quality of sponge titanium product. The metal gasket realizes stirring under high temperature, requires no condensation, solves the problem of distillation tube blockage.

[0027] Compared with the prior art, the equipment has low cost, environmental protection and harmlessness during production, and the sponge titanium produced by the equipment has a distillation yield almost reaching 100%, which fundamentally solves the problem of the distillation equipment for producing the sponge titanium.

BRIEF DESCRIPTION OF THE DRAWINGS

[0028] FIG. **1** is a structural diagram of one embodiment of equipment for producing sponge titanium in the present invention.

DETAILED DESCRIPTION OF THE EMBODIMENTS

[0029] The preferred embodiments of the present invention are further described in detail below:

[0030] A piece of equipment for producing sponge titanium, which includes a heating furnace **10** and a reactor **20** for containing a condensate, wherein a heating furnace cover **11** is arranged above the heating furnace **10**, a reactor cover **21** is arranged above the reactor **20**, the heating furnace cover **11** is connected with the reactor cover **21** by a pipe **40**, a resistance wire **43** is arranged on the pipe **40**, each lifting device **30** is arranged above the heating furnace cover **11** and the reactor cover **21**, a vacuum-pumping pipe **22** is arranged above a heater cover **21**, and a first metal gasket and a second metal gasket **25** are respectively arranged between two ends of the pipe **40** and the heating furnace cover **11** and the reactor cover **21**.

[0031] The inner wall of the reactor **20** is provided with a metal crucible **26** and a water-cooling jacket **27** for cooling. A first thermocouple **13** and an insulation material **12** are arranged on the heating furnace cover **11**.

[0032] The reactor cover **21** is also provided with a locking mechanism **24** fixedly connected with the reactor **20** and a locking cylinder **23** for providing power for the locking mechanism **24**.

[0033] The lifting device **30** includes a vertical lifting structure **31** connected with the heating furnace cover **11** or the reactor cover **21**, a lifting hydraulic cylinder **35** for providing power and a hydraulic steering motor **32** for adjusting the lifting hydraulic cylinder **35** are arranged below the vertical lifting structure **31**.

[0034] The upper and lower ends of the pipe **40** are provided with metal sealing rings **44**.

[0035] A touch screen **33** and an electric cabinet **34** for controlling the movement of the lifting device **30** are arranged above the lifting hydraulic cylinder **35**.

[0036] A pivoting support **36** is arranged below the electric cabinet **34**.

[0037] The pipe **40** is provided with a second thermocouple **41** and an insulation layer **42** orderly.

[0038] Scheme 1: a method for preparing titanium from potassium fluotitanate with aluminothermic reduction process

[0039] Equation involved: $3K_2TiF_6+4Al=3Ti+6KF+4AlF_3$

Embodiment 1

[0040] Under a vacuum condition, 36 g of aluminum and 240 g of potassium fluoroaluminate are reacted at 800° C.;

[0041] in a vacuum state, the reactant is distilled in the heating furnace at 1000° C., the resulting KF and AlF_3 are introduced into the reactor through the pipe;

[0042] 50.22 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 90.8% and the reduction rate is 95%.

Embodiment 2

[0043] Under a vacuum condition, 40 g of aluminum and 240 g of potassium fluoroaluminate are reacted at 800° C.;

[0044] in a vacuum state, the reactant is distilled in the heating furnace at 1000° C., the resulting KF and AlF_3 are introduced into the reactor through the pipe;

[0045] 48.39 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 97% and the reduction rate is 97.8%.

Embodiment 3

[0046] Under a vacuum condition, 44 g of aluminum and 240 g of potassium fluoroaluminate are reacted at 800° C.;

[0047] in a vacuum state, the reactant is distilled in the heating furnace at 1000° C., the resulting KF and AlF_3 are introduced into the reactor through the pipe;

[0048] 48.29 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 98.6% and the reduction rate is 99.2%.

TABLE 1

Distillation test data

Embodi-ment	Amount of added raw material, g K_2TiF_6	Al	Theoretical Ti quantity, g	Obtained sponge titanium product, g	Ti content of product, %	Reduction rate, %
1	240	36	48	50.22	90.8	95
2	240	40	48	48.39	97	97.8
3	240	44	48	48.29	98.6	99.2

[0049] Reduction rate (%)=obtained sponge titanium product*Ti content of product)/theoretical Ti quantity

[0050] Scheme 2: a method for preparing sponge titanium from potassium fluotitanate with magnesiothermic reduction process

[0051] Equation involved:

[0052] $K_2TiF_6+2Mg=Ti+2MgF_2+2KF$

Embodiment 4

[0053] Under the condition of vacuum introduction of argon, 48 g of magnesium and 240 g of potassium fluoroaluminate are reacted at 750° C.;

[0054] in a vacuum state, the reactant is distilled in the heating furnace at 1100° C., the resulting KF and MgF_2 and Mg are introduced into the reactor through the pipe;

[0055] 48.93 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 87.5% and the reduction rate is 89.2%.

Embodiment 5

[0056] Under the condition of vacuum introduction of argon, 24 g of magnesium and 240 g of potassium fluoroaluminate are reacted at 750° C.;

[0057] in a vacuum state, the reactant is distilled in the heating furnace at 1100° C., the resulting KF, AlF_3, MgF_2 and Mg are introduced into the reactor through the pipe;

[0058] 23.90 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 92.5% and the reduction rate is 92.1%.

Embodiment 6

[0059] Under the condition of vacuum introduction of argon, 12 g of magnesium and 240 g of potassium fluoroaluminate are reacted at 750° C.;

[0060] in a vacuum state, the reactant is distilled in the heating furnace at 1100° C., the resulting KF, MgF_2 and Mg are introduced into the reactor through the pipe;

[0061] 11.89g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 99.2% and the reduction rate is 98.3%.

Embodiment 7

[0062] Under the condition of vacuum introduction of argon, 6 g of magnesium and 240 g of potassium fluoroaluminate are reacted at 750° C.;

[0063] in a vacuum state, the reactant is distilled in the heating furnace at 1100° C., the resulting KF, MgF_2 and Mg are introduced into the reactor through the pipe;

[0064] 6.33 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 91.6% and the reduction rate is 96.7%.

TABLE 2

Distillation test data

Embodiment	Amount of added raw material, g: K_2TiF_6	Amount of added raw material, g: Mg	Theoretical Ti quantity, g	Obtained sponge titanium product, g	Ti content of product, %	Reduction rate, %
4	240	48	48	48.93	87.5	89.2
5	240	24	24	23.90	92.5	92.1
6	240	12	12	11.89	99.2	98.3
7	240	6	6	6.33	91.6	96.7

[0065] Scheme 3: a method for preparing sponge titanium from potassium fluotitanate with aluminum magnesium thermal reduction process

[0066] Chemical equations involved:

[0067] $3K_2TiF_6+4Al=3Ti+6KF+4AlF_3$

[0068] $K_2TiF_6+2Mg=Ti+2MgF_2+2KF$

Embodiment 10

[0069] Under the condition of vacuum introduction of argon, 36 g of aluminum, 36 g of magnesium and 240 g of potassium fluoroaluminate are reacted at 800° C.;

[0070] in a vacuum state, the reactant is distilled in the heating furnace at 1100° C., the resulting KF, AlF_3, MgF_2 and Mg are introduced into the reactor through the pipe;

[0071] 45.12 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 96.5% and the reduction rate is 90.7%.

Embodiment 11

[0072] Under the condition of vacuum introduction of argon, 36 g of aluminum, 18 g of magnesium and 240 g of potassium fluoroaluminate are reacted at 800° C.;

[0073] in a vacuum state, the reactant is distilled in the heating furnace at 1100° C., the resulting KF, AlF_3, MgF_2 and Mg are introduced into the reactor through the pipe;

[0074] 45.45 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 98% and the reduction rate is 92.8%.

Embodiment 12

[0075] Under the condition of vacuum introduction of argon, 36 g of aluminum, 9 g of magnesium and 240 g of potassium fluoroaluminate are reacted at 800° C.;

[0076] in a vacuum state, the reactant is distilled in the heating furnace at 1100° C., the resulting KF, AlF_3, MgF_2 and Mg are introduced into the reactor through the pipe;

[0077] 47.9 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 99.5% and the reduction rate is 99.3%.

Embodiment 13

[0078] Under the condition of vacuum introduction of argon, 36 g of aluminum, 2 g of magnesium and 144 g of zinc are mixed, then reacted with 240 g of potassium fluoroaluminate at 800° C.;

[0079] in a vacuum state, the reactant is distilled in the heating furnace at 1100° C., the resulting KF, AlF_3, MgF_2 and Mg are introduced into the reactor through the pipe;

[0080] 48.29 g of sponge titanium is obtained by keeping the vacuum state after cooling, the content of titanium in the product is 98.9% and the reduction rate is 99.5%.

TABLE 3

Distillation test data

Embodiment	Amount of added raw material, g: K_2TiF_6	Amount of added raw material, g: Al	Amount of added raw material, g: Mg	Theoretical Ti quantity, g	Obtained sponge titanium	Ti content of product, %	Reduction rate, %
5	240	36	36	48	45.12	96.5	90.7
6	240	36	18	48	45.45	98	92.8
7	240	36	9	48	47.9	99.5	99.3
8	240	36	2	48	48.29	98.9	99.5

[0081] From the above, we can see that the reduction rate and productivity of the sponge titanium produced by the distillation equipment for producing sponge titanium of the present invention are greatly improved.

[0082] The above is the further detailed description made to the invention in conjunction with specific preferred embodiments, but it should not be considered that the specific embodiments of the invention are only limited to the these descriptions. For one of ordinary skill in the art to which the invention belongs, many simple deductions and replacements can be made without departing from the inventive concept. Such deductions and replacements should fall within the scope of protection of the invention.

What is claimed is:

1. A distillation equipment for producing sponge titanium, comprising: a heating furnace and a reactor for containing a condensate, wherein a heating furnace cover is arranged above the heating furnace, a reactor cover is arranged above the reactor, the heating furnace cover is connected with the reactor cover by a pipe, a resistance wire is arranged on the pipe, each lifting device is arranged above the heating furnace cover and the reactor cover, a vacuum-pumping pipe is arranged above a heater cover, and a first metal gasket and a second metal gasket are respectively arranged between two ends of the pipe and the heating furnace cover and the reactor cover.

2. The distillation equipment for producing sponge titanium according to claim **1**, wherein the first metal gasket has a softening point of 900° C. and a melting point of 1000° C., and the second metal gasket has a softening point of 1100° C. and a melting point of 1200° C.

3. The distillation equipment for producing sponge titanium according to claim **2**, wherein a touch screen and an electric cabinet for controlling the movement of the lifting device are arranged above the lifting hydraulic cylinder.

4. The distillation equipment for producing sponge titanium according to claim **3**, wherein a pivoting support is arranged below the electric cabinet.

5. The distillation equipment for producing sponge titanium according to claim **1**, wherein the inner wall of the reactor is provided with a metal crucible and a water-cooling jacket for cooling.

6. The distillation equipment for producing sponge titanium according to claim **5**, wherein a touch screen and an electric cabinet for controlling the movement of the lifting device are arranged above the lifting hydraulic cylinder.

7. The distillation equipment for producing sponge titanium according to claim **6**, wherein a pivoting support is arranged below the electric cabinet.

8. The distillation equipment for producing sponge titanium according to claim **1**, wherein the reactor cover is also provided with a locking mechanism fixedly connected with the reactor and a locking cylinder for providing power for the locking mechanism.

9. The distillation equipment for producing sponge titanium according to claim **1**, wherein the lifting device comprises a vertical lifting structure connected with the reactor cover, a lifting hydraulic cylinder for providing power and a hydraulic steering motor for adjusting the lifting hydraulic cylinder are arranged below the vertical lifting structure.

10. The distillation equipment for producing sponge titanium according to claim **1**, wherein a first thermocouple and an insulation material are arranged on the heating furnace cover.

11. The distillation equipment for producing sponge titanium according to claim **1**, wherein the upper and lower ends of the pipe are provided with metal sealing rings.

12. The distillation equipment for producing sponge titanium according to claim **11**, wherein the pipe is provided with a second thermocouple and an insulation layer orderly.

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