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(54) FUEL CELL AND FUEL CELL SYSTEM AS DESCRIBED AND CLAIMED IN

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(57) ABSTRACT

A fuel cell has a membrane electrode assembly (MEA), a supply member for supplying an anode fluid to the MEA, and a gas diffusion layer provide between the Supply member and the MEA. The MEA has an electrolyte membrane and an anode catalyst. The Supply member has at least one anode fluid flow path for supplying the anode fluid toward the MEA. The anode fluid flow path has an opening provided on a discharge side thereof for the anode fluid. A space for storing a gas pushed by the supply of the anode fluid is disposed between the opening of the anode fluid flow path and the gas diffusion layer so that the opening of the anode fluid flow path and the gas diffusion layer are not in direct contact with one another.

17 Claims, 10 Drawing Sheets

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FIG. 1

FIG. $\boldsymbol{6}$

FIG. 13

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FUEL CELL AND FUEL CELL SYSTEMAS DESCRIBED AND CLAIMED IN

CROSS-REFERENCE to RELATED APPLICATIONS

This application is a U.S. national stage application of International Application No. PCT/JP2009/068033 filed Oct. 19, 2009, claiming a priority date of Oct. 28, 2008, and published in a non-English language.

BACKGROUND OF THE INVENTION

1. Technical Field

This invention relates to a fuel cell comprising an electro-15 lyte membrane and an anode catalyst and a cathode catalyst provided on both sides of the electrolyte membrane, and to a fuel cell system including the fuel cell.

2. Background Art

A fuel cell has a membrane electrode assembly (hereinafter 20 referred to as MEA) provided with an electrolyte membrane, and an anode catalyst and a cathode catalyst provided on both sides of the electrolyte membrane. The fuel cell includes an anode member (anode) provided with an anode fluid flow path for Supplying an anode fluid to the anode catalyst of the 25 MEA via a gas diffusion layer, and a cathode member (cath ode) provided with a cathode fluid flow path for supplying a cathode fluid to the cathode catalyst of the MEA.

With such a fuel cell, air in the atmosphere (particularly, nitrogen which is an inert gas) mixes into the anode side as an 30 impure gas via the electrolyte membrane when power gen eration is stopped. The problem arises here that even when an operation is started in this state and a hydrogen-rich anode fluid is introduced, hydrogen is not replaced immediately, and a sufficient electrical output (or amount of power generation) 35 cannot be obtained. When the fuel cell is allowed to stand for a long term, in particular, the problem occurs that the partial pressure of the impure gas mixed into the anode rises, decreasing the amount of power generation.

To deal with these problems, a technology for purging the 40 impure gas, which has been accumulated in the anode, with the hydrogen-rich anode fluid before start of operation has been proposed (see, for example, Patent Document 1).

Concretely, Patent Document 1 involves a purge valve for purging an impure gas accumulated in an anode with a hydro- 45 gen-rich anode fluid, and an exhaust gas treatment device for diluting an exhaust gas, which is discharged through the purge valve and contains hydrogen, and discharging the diluted gas to the outside.

According to this constitution of Patent Document 1, the 50 impure gas on the anode side can be replaced by the hydro gen-rich anode fluid. Thus, a decrease in the amount of power generation can be prevented.

PRIOR ART DOCUMENT

Patent Document

[Patent Document 1] JP-A-2004-193107

I he constitution of Patent Document \mathbf{I} , however, needs the $\mathbf{60}$ purge valve and the exhaust gas treatment device, and is confronted with the problem that it results in the upsizing of equipment and a cost increase.

With the constitution of Patent Document 1, moreover, the impure gas can be excluded from the anode by purging at the 65 starting of the equipment. However, the impure gas passes into the anode through the electrolyte membrane even during

power generation. Thus, during long-term power generation, the opening and closing of the purge Valve must be controlled, with the status of power generation being monitored, posing the problem of complicated control.

SUMMARY OF THE INVENTION

10 present invention to provide a downsized fuel cell and a The present invention has been accomplished in the light of the above-described circumstances. It is an object of the downsized fuel cell system which can prevent a power generation failure due to the impure gas and can perform power generation continuously for a long term.

A first aspect of the present invention for solving the above problems is a fuel cell, comprising: a membrane electrode assembly equipped with an electrolyte membrane and an anode catalyst; and a supply member for supplying an anode fluid to the membrane electrode assembly, and wherein the supply member is provided with an anode fluid flow path for supplying the anode fluid toward the membrane electrode assembly, and an opening of the anode fluid flow path on a discharge side thereof for the anode fluid is provided in proximity to the membrane electrode assembly, with a predeter-
mined space being disposed between the supply member and
the membrane electrode assembly, the predetermined space being adapted to store a gas pushed away by supply of the anode fluid.

According to the first aspect mentioned above, the anode fluid is supplied toward the membrane electrode assembly by the anode fluid flow path. By so doing, the impure gas present on the surface of the anode catalyst can be pushed away by the anode fluid, and the anode fluid can be supplied uniformly throughout the surface of the anode catalyst. By this means, the amount of power generation, particularly, the initial voltage, can be rendered high, and power generation can be maintained for a long term.

A second aspect of the present invention is the fuel cell according to the first aspect, wherein the supply member is provided with a protruding portion which protrudes toward the membrane electrode assembly and within which the

According to the second aspect mentioned above, by providing the protruding portion, the space is defined between the membrane electrode assembly and the supply member in the region other than the protruding portion. Thus, the impure gas is easily pushed away into this space. Moreover, a large amount of the impure gas can be stored within the space, so that power generation can be continued for an even longer term.

A third aspect of the present invention is the fuel cell according to the second aspect, wherein the protruding por tion has a tapered shape pointed toward the membrane elec trode assembly.
According to the third aspect mentioned above, the pro-

According to the third aspect mentioned above, the pro-
55 truding portion is pointed, whereby a large space can be defined in the region other than the protruding portion. Thus, an even larger amount of the impure gas can be stored within the space.

A fourth aspect of the present invention is the fuel cell according to any one of the first to third aspects, wherein the anode fluid flow path has a tapered shape pointed toward the

According to the fourth aspect mentioned above, the anode fluid flow path is pointed, whereby the flow velocity of the anode fluid jetted from the anode fluid flow path is increased, and the impure gas present on the Surface of the anode catalyst can be pushed away by the anode fluid even more efficiently.

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A fifth aspect of the present invention is the fuel cell according to any one of the first to fourth aspects, wherein a plurality of the anode fluid flow paths are provided in the single supply member.

According to the fifth aspect mentioned above, the anode fluid can be supplied uniformly to the surface of the anode catalyst having a relatively large area by the plurality of anode fluid flow paths.

A sixth aspect of the present invention is the fuel cell according to any one of the first to fourth aspects, wherein a 10 plurality of the anode fluid flow paths are provided in the single supply member, there are provided a chamber communicating with the plurality of anode fluid flow paths on a side opposite to the membrane electrode assembly, and an anode fluid introduction port for supplying the anode fluid to the 15 chamber, the supply member is provided with a protruding portion which protrudes toward the membrane electrode assembly and within which the anode fluid flow path is provided, the protruding portion having a first protruding portion and a second protruding portion, and the second protruding portion is at a longer distance from the anode fluid introduc tion port thana distance from the anode fluid introduction port to the first protruding portion, and an amount of protrusion of the first protruding portion is larger than an amount of protrusion of the second protruding portion. 25

According to the sixth aspect mentioned above, the pressures of the anode fluid jetted from the plurality of anode fluid flow paths are uniformized, so that the anode fluid can be supplied uniformly to the surface of the anode catalyst.

A seventh aspect of the present invention is the fuel cell 30 according to any one of the first to sixth aspects, further comprising a chamber communicating with a plurality of the anode fluid flow paths on a side opposite to the membrane electrode assembly, and an anode fluid introduction port for supplying the anode fluid to the chamber, and wherein a 35 pressure loss in the anode fluid flow path is greater than a pressure loss in an area from the anode fluid introduction port

According to the seventh aspect mentioned above, the anode fluid can be vigorously ejected from the anode fluid 40 according to the eleventh aspect, wherein the removal means flow path to blow off the impure gas present on the surface of the anode catalyst.

An eighth aspect of the present invention is the fuel cell according to any one of the fifth to seventh aspects, further comprising a chamber communicating with the plurality of 45 anode fluid flow paths on a side opposite to the membrane electrode assembly, and an anode fluid introduction port for supplying the anode fluid to the chamber, and wherein the plurality of anode fluid flow paths include a first of the anode μ muid flow paths, and a second of the anode fluid flow paths μ whose distance from the anode fluid introduction port is longer than a distance from the anode fluid introduction port to the first anode fluid flow path, and a pressure loss in the first anode fluid flow path is greater than a pressure loss in the

According to the eighth aspect mentioned above, the pressures of the anode fluid jetted from the plurality of anode fluid flow paths are uniformized, so that the anode fluid can be supplied uniformly to the surface of the anode catalyst.

A ninth aspect of the present invention is the fuel cell 60 according to any one of the fifth to eighth aspects, further comprising a chamber communicating with the plurality of anode fluid flow paths on a side opposite to the membrane electrode assembly, and an anode fluid introduction port for supplying the anode fluid to the chamber, and wherein the 65 plurality of anode fluid flow paths include a first of the anode fluid flow paths, and a second of the anode fluid flow paths

whose distance from the anode fluid introduction port is longer than a distance from the anode fluid introduction port to the first anode fluid flow path, and a pressure loss in a first guide path within the chamber in an area from the anode fluid introduction port to the first anode fluid flow path is greater thana pressure loss in a second guide path within the chamber in an area from the anode fluid introduction port to the second anode fluid flow path.

According to the ninth aspect mentioned above, the pres sures of the anode fluid jetted from the plurality of anode fluid flow paths are uniformized, so that the anode fluid can be supplied uniformly to the surface of the anode catalyst.

A tenth aspect of the present invention is the fuel cell according to the eighth aspect, wherein spacings between the adjacent anode fluid flow paths of the plurality of anode fluid flow paths of the supply member gradually decrease from the anode fluid flow paths at shorter distances from the anode fluid introduction port toward the anode fluid flow paths at longer distances from the anode fluid introduction port.

By varying the pressure losses in the anode fluid flow paths, variations occur in the flow velocity of the anode fluid, and the range of spread of the anode fluid differs according to the distribution of the flow velocity. According to the tenth aspect mentioned above, however, the spacings between the adja cent anode fluid flow paths are varied, whereby the uneven ness in the in-plane distribution of the anode fluid can be reduced.

An eleventh aspect of the present invention is the fuel cell according to any one of the first to tenth aspects, further comprising removal means for removing the gas from the

region storing the gas pushed away by the anode fluid.
According to the eleventh aspect mentioned above, the gas, such as an impure gas, pushed away within the space charged with the anode fluid can be removed from the space charged with the anode fluid. Thus, the amount of power generation can be increased further, and power generation can be main tained for a long term.

A twelfth aspect of the present invention is the fuel cell is a lead-out path which communicates with the region storing the gas pushed away by the Supply of the anode fluid to discharge the gas as a buffer.
According to the twelfth aspect mentioned above, the gas

such as an impure gas can be discharged via the lead-out path as a buffer. Thus, the amount of power generation can be increased further, and power generation can be maintained for a long term.

A thirteenth aspect of the present invention is the fuel cell according to the twelfth aspect, wherein the lead-out path is provided with a check valve which permits a flow of the gas from the region storing the gas to the buffer and restrains a flow of the gas in a reverse direction.

According to the thirteenth aspect mentioned above, the gas discharged to the buffer does not return because of the check valve. Thus, the amount of power generation can be increased further, and power generation can be maintained for a long term.

A fourteenth aspect of the present invention is the fuel cell according to the eleventh aspect, wherein the removal means is an adsorbent provided in the region storing the gas pushed away by the anode fluid.

According to the fourteenth aspect mentioned above, the gas, Such as an impure gas, is selectively adsorbed to the adsorbent, and can be removed thereby. Thus, the amount of power generation can be increased further, and power gen eration can be maintained for a long term.

(Embodiment 1)

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A fifteenth aspect of the present invention is a fuel cell system, comprising: the fuel cell according to any one of the first to fourteenth aspects; and fuel supply means for supplying the anode fluid to the fuel cell.

According to the fifteenth aspect mentioned above, a fuel cell system can be realized which prevents a power generation failure due to an impure gas, which can perform power gen eration continuously for a long term, and which has been downsized.

With the present invention, the anode fluid is flowed toward $\frac{10}{10}$ the membrane electrode assembly by the anode fluid flow path. By so doing, the impure gas on the Surface of the anode catalyst is pushed away, and the anode fluid can be supplied throughout the surface of the anode catalyst. Thus, there is no need to provide a complicated mechanism such as a purge valve or a gas treatment device. Also, a power generation failure, or a decrease in the amount of power generation, due to the impure gas is prevented, the amount of power genera tion is increased, and long-term power generation can be maintained. Moreover, it suffices to provide the anode fluid flow path for flowing the anode fluid toward the membrane electrode assembly. Thus, the provision of a purge valve, or a procedure such as complicated opening and closing of the purge valve becomes unnecessary, downsizing can be achieved, and the cost can be reduced. 25

BRIEF DESCRIPTION OF THE DRAWINGS

FIG. 1 is a block diagram showing the schematic configu ration of a fuel cell system according to Embodiment 1 of the 30 present invention.

FIG. 2 is an exploded perspective view showing the fuel cell according to Embodiment 1 of the present invention.

FIG.3 is a sectional view showing the fuel cell according to Embodiment 1 of the present invention.

FIG. 4 is a sectional view of essential parts showing the supply state of an anode fluid in the fuel cell according to Embodiment 1 of the present invention.

FIG. 5 is a sectional view of essential parts of a fuel cell according to Embodiment 2 of the present invention.

FIG. 6 is a sectional view of essential parts of another example of the fuel cell according to Embodiment 2 of the present invention.

FIG. 7 is a plan view of essential parts of a fuel cell according to another embodiment of the present invention.

FIG. 8 is a plan view of essential parts of a fuel cell according to still another embodiment of the present inven tion.

FIG. 9 is a sectional view of essential parts of the fuel cell according to the still another embodiment of the present 50 invention.

FIG. 10 is a plan view of essential parts of a fuel cell according to a further embodiment of the present invention.

FIG. 11 is a sectional view of essential parts of a fuel cell according to a still further embodiment of the present inven-55 tion.

FIG. 12 is a sectional view of essential parts of a fuel cell according to an additional embodiment of the present inven tion.

FIG. 13 is a sectional view of essential parts of a fuel cell $\frac{60}{2}$ according to a further additional embodiment of the present invention.

DETAILED DESCRIPTION Of the INVENTION

Hereinbelow, the present invention will be described in detail based on its embodiments.

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FIG. 1 is a view showing the schematic configuration of a fuel cell system according to the present invention.
As shown in FIG. 1, a fuel cell system 1 of the present

embodiment comprises a fuel supply means 100, a fuel cell 200, and a control circuit 300.

The fuel supply means 100 supplies a fuel as an anode fluid to the fuel cell 200. Hydrogen is optimal as the fuel, and a hydrogen absorbing or storage alloy, a cylinder enclosing hydrogen, etc. are named as the fuel supply means 100. The fuel supply means 100 may be one for gene rating hydrogen, and an example thereof is of a configuration in which a hydrogen generating substance and a hydrogen generation accelerator are mixed to produce hydrogen. For example, sodium borohydride can be used as the hydrogen generating substance, and an aqueous solution of malic acid can be used as the hydrogen generation accelerator. Moreover, a solution of methanol may be supplied as the fuel.

The control circuit 300 is connected to the fuel cell 200 , and driven by a voltage supplied by the fuel cell 200.

The fuel cell 200 will be described in detail by reference to FIGS. 2 to 4. FIG. 2 is an exploded perspective view showing the schematic configuration of the fuel cell. FIG. 3 is a sec tional view of the fuel cell. FIG. 4 is a sectional view of essential parts showing the Supply state of the anode fluid in the fuel cell.

As shown in FIGS. 2 and 3, the fuel cell 200 has a mem brane electrode assembly 204 (hereinafter referred to as MEA) composed of a solid polymer electrolyte membrane 201 as an electrolyte membrane, and an anode catalyst 202 and a cathode catalyst 203 provided on both sides of the solid polymer electrolyte membrane 201.

35 the MEA 204 is sandwiched between the anode member 210 An anode member 210 and a cathode member 220 are provided on the respective surfaces of the MEA 204. That is, and the cathode member 220.

ode catalyst 203 is located. The cathode member 220 is pro-
40 vided with a cathode fluid flow path 221 for supplying an The cathode member 220 is composed of a plate-shaped member provided on a side of the MEA 204 where the cath-
ode catalyst 203 is located. The cathode member 220 is prooxidizing agent (air containing oxygen), as a cathode fluid, to the cathode catalyst 203. That is, the cathode member 220 functions as a supply member for supplying the cathode fluid to the cathode catalyst 203. The cathode fluid flow path 221, in the present embodiment, has a concave shape opening at a side of the cathode member 220 facing the cathode catalyst 203. In the bottom surface of the cathode fluid flow path 221, a cathode fluid introduction port 222 is provided for supply ing air into the cathode fluid flow path 221.

The anode member 210 is composed of a plate-shaped member provided on a side of the MEA 204 where the anode catalyst 202 is located. The anode member 210 has a chamber 211 of a concave shape opening toward the anode catalyst 202, and an anode fluid introduction port 212 provided as a through-hole in the thickness direction of the bottom surface of the chamber 211.

The chamber 211 has an opening area comparable to the surface area of the anode catalyst 202. The interior of the chamber 211 is supplied with the anode fluid via the anode fluid introduction port 212 provided in the bottom surface thereof.

Between the anode member 210 and the MEA 204, there are provided a gas diffusion layer 230, and a supply member 240 for supplying the anode fluid within the chamber 211 to the gas diffusion layer 230.

The gas diffusion layer (GDL) 230 is provided between the anode member 210 and the MEA 204 to face the MEA 204, 10

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that is, to be located on the anode catalyst 202 of the MEA 204, and comprises a member having permeability which allows the anode fluid to pass therethrough. As the gas diffu sion layer 230, a well-known material can be used, for example, a metal mesh or a material having a porous structure such as a carbon cloth, a carbon paper, or a carbon felt.

The supply member 240 comprises a plate-shaped member provided on a side opposite to the MEA 204 across the gas diffusion layer 230. The supply member 240 is disposed in such a state as to be separated from the gas diffusion layer 230 by a predetermined spacing, and a predetermined space 250 is defined between the supply member 240 and the gas diffusion layer 230. A surface of the supply member 240 on a side opposite to the gas diffusion layer 230 seals one surface of the chamber 211.

The supply member 240 is provided with an anode fluid flow path 241 to penetrate the supply member 240 in its thickness direction, thereby bringing the chamber 211 and the space 250 into communication. That is, the anode fluid flow path 241 has one end opening into the chamber 211 and the other end opening into the space 250, thereby establishing communication between them. As described above, the one surface of the supply member 240 is not brought into contact with the gas diffusion layer 230, but is separated therefrom by a predetermined spacing. Because of this configuration, the 25 one surface of the supply member 240 is provided in proxim ity to the anode catalyst 202, with the space 250 being dis posed between the opening of the anode fluid flow path 241 on its discharge side for the anode fluid (the opening facing the gas diffusion layer 230) and the gas diffusion layer 230. 30

In the present embodiment, there are provided two rows of the anode fluid flow paths 241, each row including a plurality of (six) the anode fluid flow paths 241 arranged with prede termined spacing, so that 12 of the anode fluid flow paths 241 are provided. The anode fluid flow path 241 is provided such 35 that a pressure loss in the anode fluid flow path 241 is greater than a pressure loss occurring in a region ranging from the anode fluid introduction port 212 to each anode fluid flow path 241. Concretely, in the present embodiment, the cham ber 211 is provided to be of such a size as to be in common 40 communication with the plurality of anode fluid flow paths 241 (namely, the opening area of the chamber 211 is compa rable to the surface area of the anode catalyst 202), and the opening areas (cross-sectional areas) of the anode fluid flow paths 241 are much Smaller than the opening area of the 45 chamber 211. Consequently, the pressure loss in the anode fluid flow path 241 is rendered greater than the pressure loss occurring in the region ranging from the anode fluid intro duction port 212 of the chamber 211 to each anode fluid flow path 241. By so increasing the pressure loss in the anode fluid 50 flow path 241, the anode fluid supplied into the chamber 211 can be Supplied as jets at a desired pressure toward the Surface of the anode catalyst 202 by the anode fluid flow path 241, although the details of this action will be described later. The anode fluid flow path 241 may be of a shape pointed toward 55 the anode catalyst 202. Of course, the anode fluid flow path 241 is not limited in size (opening area), number or position, and the size, number and position may be determined, as appropriate, based on the pressure of the anode fluid within the chamber 211, the partial pressure of an impure gas on the 60 surface side of the anode catalyst 202, the flow velocity of the anode fluid supplied to the anode catalyst 202 to push away the impure gas, and so on. If the anode fluid flow path 241 is shaped to be pointed or tapered toward the anode catalyst 202, as mentioned above, the flow velocity of the anode fluid jetted 65 from the anode fluid flow path 241 can be increased. By so doing, the anode fluid can be easily supplied to the surface of

the anode catalyst 202; that is, the impure gas existent on the surface of the anode catalyst 202 can be easily pushed away, although the details will be offered later.

The anode fluid flow path 241 of the supply member 240 penetrates the supply member 240 in its thickness direction, and is thereby provided along a direction intersecting the surface of the anode catalyst 202. By this measure, the anode fluid supplied into the chamber 211 can be passed through the gas diffusion layer 230 by way of the anode fluid flow path 241, and supplied as jets toward the surface of the anode catalyst 202. That is, it suffices for the anode fluid flow path 241 of the supply member 240 to be provided along the direction intersecting the surface of the anode catalyst 202. The anode fluid flow path 241 may be orthogonal to the surface of the anode catalyst 202, or may be inclined at a predetermined angle with respect to this surface.

With the above-described fuel cell 200, the cathode fluid flow path 221 is open to the atmosphere. If the fuel cell is allowed to stand for a long term, therefore, air in the atmo sphere (particularly, nitrogen as an inert gas) slips, as an impure gas, into a space where the anode catalyst 202 is provided, i.e., within the gas diffusion layer 230 or the space 250, through the solid polymer electrolyte membrane 201. Arise in the partial pressure of the impure gas (nitrogen) causes a drop in the partial pressure of the anode fluid in the anode catalyst 202. Thus, a sufficient amount of the anode fluid for power generation cannot be Supplied, so that the amount of power generation decreases.

With the fuel cell 200 of the present embodiment, however, the anode fluid is supplied by the anode fluid flow paths 241 to be blown toward the surface of the anode catalyst 202, as shown in FIG. 4. Thus, the impure gas existent on the surface of the anode catalyst 202 is pushed away, and the anode fluid can be supplied to the surface of the anode catalyst 202. That is, the anode fluid supplied by the anode fluid flow paths 241 toward the surface of the anode catalyst 202 (from the direc tion intersecting the Surface) spreads along the Surface of the anode catalyst 202 while pushing away the impure gas within the gas diffusion layer 230 filled as an atmosphere for the anode catalyst 202. On this occasion, the impure gas pushed away from the surface side of the anode catalyst 202 remains in regions on a side of the gas diffusion layer 230 opposite to the anode catalyst 202, and within the space 250, namely, in regions A shown in FIG. 4. Since the space 250 is present, the impure gas is easily pushed away from the Surface of the anode catalyst 202.

As described above, the anode fluid is supplied toward the surface of the anode catalyst 202 by the anode fluid flow paths 241 to push away the impure gas (nitrogen) from the surface of the anode catalyst 202, whereby the efficiency of power generation or the power efficiency of the anode catalyst 202 can be increased. For example, if the anode fluid flow path 241 is not provided, namely, if the chamber 211 is provided to face the gas diffusion layer 230 directly, the anode fluid supplied from the anode fluid introduction port 212 is supplied along the surface of the anode catalyst 202. If the anode fluid is supplied in the planar direction of the surface of the anode catalyst 202 in this manner, power generation takes place only on the side where the anode fluid is supplied. In a region extending long from the side where the anode fluid is supplied, on the other hand, the partial pressure of the impure gas becomes so high that power generation substantially does not occur. That is, when the anode fluid is Supplied along the surface of the anode catalyst 202, the entire surface of the anode catalyst 202 cannot be used efficiently, so that the amount of power generation decreases. By contrast, the anode fluid flow path 241 supplying the anode fluid in such a manner as to blow it against the surface of the anode catalyst 202 is provided as in the present embodiment, whereby the anode fluid can be supplied uniformly over the entire surface of the anode catalyst 202. Thus, power generation can be performed with the use of the entire surface of the anode catalyst 202, 5 and the amount of power generation, particularly, the initial voltage, can be rendered high.

With the fuel cell 200, moreover, the mixing of the impure gas, Such as nitrogen in the air, into the anode catalyst 202 (gas diffusion layer 230) occurs during power generation as 10 well. Thus, long-term power generation cannot be main tained, if the anode fluid flow path 241 is not provided. In the present embodiment, on the other hand, the anode fluid is supplied toward the surface of the anode catalyst 202 by the anode fluid flow paths 241. By so doing, the anode fluid can 15 continue to be supplied to the surface of the anode catalyst 202, with the impure gas present on the surface of the anode catalyst 202 being constantly pushed away, so that long-term power generation can be maintained.

In the present embodiment, moreover, the anode fluid is 20 blown against the surface of the anode catalyst 202 by the anode fluid flow path 241. Thus, the thickness of the gas diffusion layer 230 can be rendered relatively small. Even if the gas diffusion layer 230 is not provided, the anode fluid can be supplied uniformly throughout the surface of the anode 25 catalyst 202.

(Embodiment 2)

FIG. 5 is a sectional view of essential parts of a fuel cell according to Embodiment 2 of the present invention. The according to Embodiment 2 of the present invention. The same members as those in the aforementioned Embodiment 1 30 will be assigned the same numerals as in the Embodiment 1, and duplicate explanations will be omitted.

As shown in FIG. 5, a fuel cell 200A of Embodiment 2 has an MEA 204, an anode member 210, a cathode member 220 (not shown), a gas diffusion layer 230, and a Supply member 35 240A.

A surface of the supply member 240A facing the gas dif fusion layer 230 is provided with protruding portions 242 which protrude toward the gas diffusion layer 230 and inside each of which an anode fluid flow path 241 is provided. That 40 is, the protruding portion 242 is provided in a cylindrical nozzle-like form within which the anode fluid flow path 241 is provided. The shape of the protruding portion 242 is not limited to the cylindrical form, but may be a prismatic shape, or a tapered shape which is pointed toward the MEA 204. For 45 example, the protruding portion 242 is formed in a tapered shape pointed toward the MEA 204, whereby the volume of the space between the adjacent protruding portions 242 can
be rendered larger than that of the space between the adjacent be rendered larger than that of the space between the adjacent
cylindrical protruding portions 242, and further the amount of 50 been described above. However, the basic features of the the impure gas storable in this space is increased, thereby making it possible to maintain long-term power generation. Details in this connection will be described later.

The protruding leading end surface of the protruding portion 242 is provided in such a state as to be separated from the 55 gas diffusion layer 230 by a predetermined spacing, that is, with a space 250 being disposed between the protruding portion 242 and the gas diffusion layer 230. In a region of the supply member 240A other than the protruding portion 242, a space 251 broader than the space 250 is provided between 60 the supply member 240A and the gas diffusion layer 230.

With the fuel cell 200A described above, the anode fluid is supplied toward the surface of the anode catalyst 202 by the anode fluid flow paths 241, as in the aforementioned Embodi ment 1. Thus, the impure gas such as nitrogen is pushed away, 65 so that the amount of initial power generation can be increased, and power generation can be maintained for a long

term. In the present embodiment, moreover, the wider space 251 is defined between the gas diffusion layer 230 and the supply member 240A in the region of the supply member 240A other than the protruding portion 242. By this configu ration, the impure gas such as nitrogen which has been expelled from the surface of the anode catalyst 202 can be stored in a region A' including this space 251. Thus, the impure gas on the surface side of the anode catalyst 202 is easily pushed away toward the region A'. Furthermore, the impure gas pushed away can be stored in the relatively wide region A', so that power generation of an even longer duration can be maintained.

In the present embodiment, a plurality of the protruding portions 242 having the same amount of protrusion are provided. However, this is not limitative, and the amount of protrusion of the protruding portion 242 may be varied based on the distance within the chamber 211 from the anode fluid introduction port 212 to each anode fluid flow path 241. Such an example is shown in FIG. 6. FIG. 6 is a sectional view of essential parts showing a modification of the fuel cell accord ing to Embodiment 2 of the present invention.

In the fuel cell 200A, as shown in FIG. 6, the amount of protrusion of the protruding portion 242 is larger for the anode fluid flow path 241 at a shorter distance from the anode fluid introduction port 212 in the chamber 211, while the amount of protrusion of the protruding portion 242 is smaller for the anode fluid flow path 241 at alonger distance from the anode fluid introduction port 212. In this case, the opening of the anode fluid flow path 241 provided in each protruding portion 242 is provided not to contact the gas diffusion layer 230A.

By so changing the amount of protrusion of the protruding portion 242, the pressure loss in the anode fluid flow path 241 close to the anode fluid introduction port 212 is increased, while the pressure loss in the anode fluid flow path 241 distant from the anode fluid introduction port 212 is decreased. As a result, the pressure of the anode fluid supplied from each anode fluid flow path 241 can be uniformized, regardless of the distance from the anode fluid introduction portion 212. Consequently, the amount of power generation in the plane of the anode catalyst 202 can be uniformized to increase the power efficiency.

In the present embodiment, the gas diffusion layer 230A can be rendered relatively thin, and it is permissible not to provide the gas diffusion layer 230A. Even in this case, the anode fluid can be supplied uniformly throughout the surface of the anode catalyst 202.

(Other Embodiments)

The respective embodiments of the present invention have present invention are not limited to those mentioned above.

For example, in the aforementioned Embodiments 1 and 2. the plurality of anode fluid flow paths 241 having the same opening area are provided in the supply member 240, 240A. However, this is not limitative and, for example, the pressure loss in the anode fluid flow path 241 may be varied according to the distance from the anode fluid introduction port 212. A concrete example is shown in FIG. 7. FIG. 7 illustrates a modification of the aforementioned Embodiment 1, but the configuration of FIG. 7 can be applied to the aforementioned Embodiment 2 as well. As shown in FIG. 7, of the plurality of anode fluid flow paths 241, the anode fluid flow path 241 at a shorter distance (distance L_1) from the anode fluid introduction port 212 (projected part 212A obtained by projection of the anode fluid introduction port 212) is given a smaller cross-sectional area to impart a larger pressure loss, while the anode fluid flow path 241 at a longer distance (distance L_6)

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from the anode fluid introduction port 212 is given a larger cross-sectional area to impart a smaller pressure loss. That is, let the anode fluid flow path 241 at the short distance from the anode fluid introduction port 212 be the first anode fluid flow path, and let the anode fluid flow path 241 at the long distance 5 from the anode fluid introduction port 212 be the second anode fluid flow path. In this case, the pressure loss in the first anode fluid flow path may be greater than the pressure loss in the second anode fluid flow path.

In the present embodiment, the anode fluid introduction 10 port 212 is provided in the bottom surface of the chamber 211 and outside the rows of the juxtaposed anode fluid flow paths 241. However, the anode fluid introduction port 212 may be provided halfway through the rows of the juxtaposed anode $\frac{1}{10}$ flow paths 241. The distance from the anode fluid intro- $\frac{15}{15}$ duction port 212 to the anode fluid flow path 241 may be actually taken on the premise that the position of the anode fluid introduction port 212 is the position of the projected part 212A obtained by projecting the anode fluid introduction port 212 onto the supply member 240.

As noted above, the opening area (cross-sectional area) of the anode fluid flow path 241 is varied based on the distance from the anode fluid introduction port 212, whereby the pres sure loss in the anode fluid flow path 241 can be varied based on the distance from the anode fluid introduction port 212. 25 That is, the fact that the opening area of the anode fluid flow path 241 is Small means that the pressure loss in the anode fluid flow path 241 is great, whereas the fact that the opening area of the anode fluid flow path 241 is large means that the pressure loss in the anode fluid flow path 241 is small. The 30 path within the chamber 211 from the anode fluid introduc tion port 212 to the anode fluid flow path 241 at a short distance therefrom is short. Thus, the pressure loss of the anode fluid passing along this path in the chamber 211 is small. The longer the distance over which the anode fluid 35 passes through the chamber 211 from the anode fluid intro duction port 212 until its supply to the anode fluid flow path 241, the larger its pressure loss becomes. Hence, variations in the pressure loss of the anode fluid passing within the cham ber 211 can be counterbalanced by varying the pressure loss 40 in the anode fluid flow path 241, whereby the pressure of the anode fluid supplied from each anode fluid flow path 241 can be rendered uniform. By this measure, the anode fluid can be supplied uniformly to the surface of the anode catalyst 202 to provide a uniform amount of power generation in the plane of 45 the anode catalyst 202 and increase the efficiency of power generation (i.e., power efficiency).

In the example shown in FIG. 7, the flow rate of the anode fluid supplied from each anode fluid flow path 241 can be uniformized. However, as the distance from the anode fluid $50₁$ introduction port 212 (projected part 212A obtained by pro jection of the anode fluid introduction port 212) to the anode fluid flow path 241 increases, the bore of the anode fluid flow path 241 differs, so that the flow velocity of the anode fluid flowed out of the anode fluid flow path 241 changes. If the 55 flow velocity of the anode fluid flowed out of the anode fluid flow path 241 changes in this manner, the range of spread of the anode fluid differs according to the distribution of the flow velocity. As a result, unevenness occurs in the in-plane distribution of the anode fluid, causing a possibility for a 60 decrease in the power efficiency. Thus, in the plurality of anode fluid flow paths 241, the spacing between the adjacent anode fluid flow paths 241 is gradually decreased as the distance from the anode fluid introduction port 212 increases. By so doing, the unevenness in the in-plane distribution of the 65 anode fluid can be curtailed. An example of such a configuration is shown in FIGS. 8 and 9. FIG. 8 is a plan view of

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essential parts of a fuel cell according to other embodiment of the present invention. FIG. 9 is a sectional view of essential parts of FIG. 8.

As shown in FIGS. 8 and 9, in the plurality of anode fluid flow paths 241 having the opening areas differentiated in the same manner as in FIG. 7, the spacing (e.g., spacing d_5) between the adjacent anode fluid flow paths 241 at a longer distance from the anode fluid introduction port 212 (projected part 212A) is rendered Smaller than the spacing (e.g., spacing d_1) between the adjacent anode fluid flow paths 241 at a shorter distance from the anode fluid introduction port 212 (projected part 212A). Because of this configuration, the flow velocity slows from a side where the spacing between the adjacent anode fluid flow paths 241 is wide (i.e., spacing d_1) side) toward a side where the spacing between the adjacent anode fluid flow paths 241 is narrow (i.e., spacing d_5 side). Even if the range of spread of the anode fluid flowed out gradually narrows, therefore, the unevenness in the in-plane distribution of the anode fluid can be reduced. Hence, the impure gas (nitrogen) present on the surface of the anode catalyst 202 can be uniformly pushed away from the surface of the anode catalyst 202, and power generation can be carried out with high efficiency. In this connection, assume that the spacings between the adjacent anode fluid flow paths are all set to be identical. When, in this case, the anode fluid flow path 241 at a short distance from the anode fluid introduction port 212 is taken as the first anode fluid flow path, and the anode fluid flow path 241 at a long distance from the anode fluid introduction port 212 is taken as the second anode fluid flow path, the flow velocity of the anode fluid flowing out from the second anode fluid flow path is lower than the flow velocity of the anode fluid flowing out from the first anode fluid flow path. In this state, the range in which the anode fluid of a lower flow velocity flowing out of the second anode fluid flow path pushes away the gas and spreads on the surface of the anode catalyst 202 is narrower than the range in which the anode fluid of a higher flow velocity flowing out of the first anode fluid flow path spreads on the surface of the anode catalyst 202. Consequently, unevenness occurs in the distribution of the concentration at which the anode fluid is supplied in the plane of the surface of the anode catalyst 202, posing a possibility for the occurrence of a deficiency, such as the failure to push away the impure gas, or a decrease in the power efficiency.

The example shown in FIGS. 8 and 9 can reduce the unevenness in the in-plane distribution of the anode fluid flowed out of the plurality of anode fluid flow paths 241. Thus, the distribution of the concentration at which the anode fluid is supplied in the plane of the surface of the anode catalyst 202 is uniformized, so that the power efficiency of the anode catalyst 202 can be increased, and the amount of power generation can be maintained for a long term. In the example shown in FIGS. 8 and 9, the spacings between the centers of the adjacent anode fluid flow paths 241 are taken as the spacings d_1 to d_5 between the anode fluid flow paths. However, this is not limitative, and the spacing between the edges of the openings of the anode fluid flow paths may be taken as

Furthermore, it is permissible to form a guide path within the chamber 211, the guide path serving for communication from the anode fluid introduction port 212 to the anode fluid flow path 241, and change the pressure loss in this guide path, without changing the pressure loss in the anode fluid flow path 241. Such an example is shown in FIG. 10.

As shown in FIG. 10, a guide path 213 serving for com munication from the anode fluid introduction port 212 to each anode fluid flow path 241 is provided within the chamber 211. The guide path 213 is configured such that the guide path 213 for communication from the anode fluid introduction port 212 to the anode fluid flow path 241 at a shorter distance there from has a smaller width (cross-sectional area) to undergo a larger pressure loss, and the guide path 213 for communica tion from the anode fluid introduction port 212 to the anode fluid flow path 241 at a longer distance therefrom has a larger width (cross-sectional area) to undergo a smaller pressure loss. That is, when the anode fluid flow path 241 at a short distance from the anode fluid introduction port 212 is taken as 10 the first anode fluid flow path, and the anode fluid flow path 241 at a long distance from the anode fluid introduction port 212 is taken as the second anode fluid flowpath, it is advisable that a pressure loss in the first guide path from the anode fluid introduction port 212 to the first anode fluid flow path be 15 rendered greater than a pressure loss in the second guide path from the anode fluid introduction port 212 to the second anode fluid flow path. Because of this configuration, the pres sure of the anode fluid supplied from each anode fluid flow path 241 can be uniformized. By this measure, the anode fluid can be Supplied uniformly to the Surface of the anode catalyst 202 to provide a uniform amount of power generation in the plane of the anode catalyst 202 and increase the power effi ciency.

Furthermore, in a region where the gas pushed away by the 25 anode fluid flowed out of the anode fluid flow path 241 is stored, a removal means for discharging the gas in this region to the outside may be provided. Such an example is shown in FIG. 11. FIG. 11 is a sectional view of essential parts of a fuel cell showing a modification of the aforementioned Embodi 30 ment 2.

As shown in FIG. 11, one end of a lead-out path 260 communicating with the space 251 which is a region for storing the gas pushed away by the anode fluid is connected to the supply member 240A, and the other end of the lead-out 35 path 260 is connected to a storage means 261. The storage means 261 has a space for storing the impure gas, such as nitrogen, from the space 251, and serves as a buffer to dis charge to the outside the gas stored in the space 251 connected via the lead-out path 260. A hollow member having a sealed 40 space is named, for example, as the storage means 261. By providing the storage means 261 composed of the hollow member, the pressure inside the storage means 261 becomes comparable to the pressure inside the fuel cell (chamber 211), while the action of the fuel cell is kept at a standstill. When the 45 anode fluid is flowed out of the anode fluid flow path 241, the impure gas pushed away into the space 251 by the flowed-out anode fluid is discharged to the storage means 261, as a buffer, via the lead-out path 260 under the introduction pressure of the anode fluid. Upon discharge of the impure gas in the space 50 251 to the storage means 261 as the buffer, the pressure inside the space 251 and the pressure inside the storage means 261 equal. When the action of the fuel cell is stopped, the pressure balance between the interior of the space 251 and the interior of the storage means 261 is disturbed, and the impure gas 55 within the storage means 261 returns to the space 251. In this manner, the impure gas in the space 251 is buffer-discharged to the outside of the fuel cell during the action of the fuel cell, whereby the amount of power generation (particularly, initial voltage) can be increased, and power generation can be main- 60 tained for a long term.

The hollow member has been named as an example of the storage means 261, but it is not limitative. For example, an adsorbent for adsorbing the gas may be provided within the storage means 261. For example, activated carbon, Zeolite or 65 the like can be used as the adsorbent, if it is desired to adsorb nitrogen as the gas.

A check valve may be provided in the lead-out path 260 shown in the aforementioned FIG. 11. Such an example is shown in FIG. 12. As shown in FIG. 12, a check valve 262 is provided halfway through the lead-out path 260, namely, between the supply member 240 and the storage means 261. The check valve 262 is mounted in a direction in which it permits the flow of the gas from the space 251, where the gas is stored, to the storage means 261 (buffer), and restrains the flow of the gas in the reverse direction. By providing the lead-out path 260 with the check valve 262 in this manner, the gas stored in the storage means 261 does not flow backward to the space 251 and, even when the action of the fuel cell is stopped, the gas stored in the storage means 261 does not return to the space 251. FIG. 12 shows a modification of the aforementioned Embodiment 2, but this is not limitative. For example, even the configuration of the aforementioned
Embodiment 1 without the space 251, or even the configuration shown in any of FIGS. 7 to 10 can exhibit the same effects as above, if provided with removal means for removing the gas in the region where the gas is stored.

Further, an adsorbent may be provided in the region where the gas pushed away by the Supply of the anode fluid is stored. Such an example is shown in FIG. 13. FIG. 13 is a sectional view of essential parts showing a modification of the afore mentioned Embodiment 2.
As shown in FIG. 13, the supply member 240A is provided

with an adsorbent 270 in the space 251 which is the region where the gas pushed away by the anode fluid is stored. As the adsorbent 270, activated carbon, Zeolite or the like can be used, for example, if it is desired to adsorb nitrogen as the gas. Of course, the adsorbent is not limited thereto, but its material may be determined, as appropriate, depending on the gas whose adsorption is desired.

Even with such a configuration, the gas pushed away to the space 251 is adsorbed to the adsorbent 270, and excess gas within the fuel cell can be removed, so that the amount of power generation (particularly, initial Voltage) can be increased, and power generation can be maintained for a long term. Needless to say, the adsorbent 270 may be provided in the aforementioned Embodiment 1.

Any two or more of the configurations shown in the afore mentioned configurations of FIGS. 7 to 13 may be combined.

In the above embodiments, the supply member 240, 240A has been provided as a member independent of the anode member 210. However, these members may be configured as a member in which they are provided integrally. Moreover, the supply member 240, 204A may be one in which only the region provided with the anode fluid flow path 241 is a supply member. That is, a member corresponding to any of the supply members 240, 240A of the aforementioned Embodiments 1 and 2 may be composed of a base member comprising a plate-shaped member, and a plurality of supply members fixed to the base member and having anode fluid flow paths individually provided therein.

In the above embodiments, the gas diffusion layer 230 has been provided only on the side of the anode catalyst 202. However, this is not limitative and, for example, a gas diffu sion layer 230 comparable to that on the side of the anode catalyst 202 may be provided on the side of the cathode catalyst 203 as well.

The above-described fuel cell 200, 200A can be utilized, for example, as a single cell constituting a cell stack. That is, a cell stack may beformed by stacking a plurality of the above fuel cells 200 or 200A.

INDUSTRIAL APPLICABILITY

The present invention can be utilized in the industrial field of fuel cells which uniformize the concentration distribution $\overline{\mathbf{S}}$

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of the anode fluid in the plane of the surface of the anode catalyst to increase the amount of power generation and con tinue power generation for a long term.

DESCRIPTION OF THE NUMERALS

A, A' Region

1 Fuel cell system

100 Fuel supply means

200 Fuel cell

201 Solid polymer electrolyte membrane (Electrolyte membrane)

202 Anode catalyst

203 Cathode catalyst

210 Anode member

- 212 Anode fluid introduction port
- 220 Cathode member

230, 230A Gas diffusion layer

240, 240A Supply member

242 Protruding portion

250 Space

251 Space

260 Lead-out path

261 Storage means

270 Adsorbent

300 Control circuit

The invention claimed is:

1. A fuel cell comprising:

a gas diffusion layer,

- a membrane electrode assembly comprised of an electro lyte membrane and an anode catalyst over which the gas diffusion layer is disposed; and
- a supply member having protruding portions each provided with an anode fluid flow path having an opening 35 on a discharge side thereof for supplying an anode fluid toward the membrane electrode assembly, the protruding portions and the gas diffusion layer being arranged with a space therebetween so that the protruding porwith a space therebetween so that the protruding portions do not contact, either directly or indirectly, the gas diffusion layer, the protruding portions being provided on a surface of the supply member facing the gas diffusion layer so as to protrude toward the member electrode assembly and form spaces for storing a gas pushed by the supply of the anode fluid toward the membrane electrode 45 assembly, each of the spaces being formed between two adjacent ones of the protruding portions.

2. A fuel cell according to claim 1; wherein each of the protruding portions of the Supply member is cylindrical shaped.

- 3. A fuel cell, comprising:
- a gas diffusion layer,
- a membrane electrode assembly comprised of an electro lyte membrane and an anode catalyst over which the gas diffusion layer is disposed; and
- a supply member for supplying an anode fluid to the membrane electrode assembly, the supply member having a plurality of anode fluid flow paths each having an opening provided on a discharge side thereof for supplying the anode fluid toward the membrane electrode assem- 60 bly, and a plurality of protruding portions within which the respective anode fluid flow paths are provided, the plurality of protruding portions and the gas diffusion layer being arranged with a space therebetween so that the plurality of protruding portions do not contact, either 65 directly or indirectly, the gas diffusion layer, each of the protruding portions being provided on a portion of the

surface of the supply member facing the gas diffusion layer so as to protrude toward the gas diffusion layer and form a plurality of spaces for storing a gas pushed by the supply of the anode fluid toward the membrane electrode assembly, each of the spaces being formed between two adjacent ones of the protruding portions and in a portion of the supply member other than portions of the surface on which the protruding portions are provided.

10 protruding portions has a tapered shape pointed toward the 4. A fuel cell according to claim 3; wherein each of the membrane electrode assembly.

5. A fuel cell according to claim 3; wherein each of the anode fluid flow paths has a tapered shape pointed toward the membrane electrode assembly.
6. A fuel cell according to claim 3; wherein the supply

member comprises a single supply member in which the plurality of anode fluid flow paths are provided.

7. A fuel cell according to claim 6; further comprising a chamber communicating with the plurality of anode fluid flow paths on a side opposite to the membrane electrode assembly, and an anode fluid introduction port for supplying the anode fluid to the chamber; wherein the plurality of anode fluid flow paths comprise a first anode fluid flow path and a second anode fluid flow path, a distance from the anode fluid introduction port to the second anode fluid flow path being longer than a distance from the anode fluid introduction port to the first anode fluid flow path so that a pressure loss in the first anode fluid flow path is greater than a pressure loss in the second anode fluid flow path.

8. A fuel cell according to claim 7; wherein spacings between adjacent anode fluid flow paths of the plurality of anode fluid flow paths gradually decrease from the anode fluid flow paths at shorter distances from the anode fluid introduction port toward the anode fluid flow paths at longer distances from the anode fluid introduction port.

9. A fuel cell according to claim 6; further comprising a chamber communicating with the plurality of anode fluid flow paths on a side opposite to the membrane electrode assembly, and an anode fluid introduction port for supplying the anode fluid to the chamber; wherein the plurality of anode fluid flow paths comprise a first anode fluid flow path and a second anode fluid flow path, a distance from the anode fluid introduction port to the second anode fluid flow path being longer than a distance from the anode fluid introduction port to the first anode fluid flow path; and wherein the chamber and the anode fluid flow paths are configured so that a pressure loss in a first guide path within the chamber in an area from the is greater than a pressure loss in a second guide path within the chamber in an area from the anode fluid introduction port

10. A fuel cell according to claim 3; further comprising a chamber and an anode fluid introduction port for supplying the anode fluid to the chamber; wherein the supply member comprises a single supply member in which the plurality of anode fluid flow paths are provided; and wherein the plurality of protruding portions comprise a first protruding portion and a second protruding portion, with an amount of protrusion of the first protruding portion being greater than an amount of protrusion of the second protruding portion, the second protruding portion being disposed at a greater distance from the anode fluid introduction port than a distance from the first protruding portion to the anode fluid introduction port.

11. A fuel cell according to claim 3; further comprising a chamber communicating with the plurality of the anode fluid flow paths on a side opposite to the membrane electrode assembly and an anode fluid introduction port for supplying

the anode fluid to the chamber, the anode fluid flow paths and the chamber being configured so that a pressure loss in each of the anode fluid flow paths is greater than a pressure loss in an area from the anode fluid introduction port to each of the anode fluid flow paths.

12. A fuel cell according to claim 3; further comprising removal means for removing the gas stored in the plurality of spaces.

13. A fuel cell according to claim 12; wherein the removal means comprises a lead-out path communicating with the 10 plurality of spaces for discharging the stored gas to a buffer.

14. A fuel cell according to claim 13; wherein the lead-out path is provided with a check valve that permits a flow of the stored gas from the plurality of spaces to the buffer while restraining a flow of the gas in a reverse direction.

15. A fuel cell according to claim 12; wherein the removal means comprises an adsorbent disposed in the plurality of spaces.

16. A fuel cell system comprising:

a fuel cell according to claim 3; and fuel Supply means for 20 supplying the anode fluid to the fuel cell.

17. A fuel cell according to claim 3; wherein each of the plurality of protruding portions of the Supply member is cylindrical-shaped.

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